

Brine Effluents: Characteristics, Environmental Impacts, and Their Handling

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Abstract. Brine discharge is one of the largest sources of wastewater from industrial processes. Because of the environmental impacts arising from improper treatment of brine discharge and more rigorous regulations of pollution control, industries have started to focus on waste minimization and improving the process of wastewater treatment. Several approaches have been proposed to provide a strategy for brine handling by recovering both brine and water or to remove pollutant components so it complies with environmental regulations when discharged. One of the most promising alternatives to brine disposal is reusing the brine, which results in reduction of pollution, minimizing waste volume and salt recovery. The brine may also contain valuable components that could be recovered for profitable use. Also, water recovery from brine effluent is generally performed to save water. In the case of rejected brine from desalination plants, water recovery from higher brine concentrations has huge potential for salt production. This paper gives an overview of different types of brine effluents, their sources and characteristics. Also discussed are impacts of brine on the environment and management options related to their characteristics.

Keywords: ballast water; brine disposal; desalination; spent regenerant; wastewater.

1 Introduction

Recently, due to the rapid growth in industrial activities, the world is facing a challenge in maintaining water supply, including protection of its quality and resources. Since the supply of quality water is decreasing, there is a growing need for wastewater reuse and recycling from industrial effluent. Meanwhile, to meet the stringent regulations of pollution control, industrial wastewater treatment techniques are evolving rapidly in view of various environmental issues. One of the largest sources of wastewater from industrial processes is brine discharge. Brine effluents are generated from various processes, such as: (1) desalination, (2) spent brine from ion-exchange regeneration, (3) ballast water, etc. Brine effluents have a strong negative impact on the environment due to their high concentration of salts and other pollutant contents [1-5]. The types of pollutants vary depending on the source. As for the aforementioned examples, desalination concentrates contain a higher salt concentration than

Received March 4th, 2016, 1st Revision April 29th, 2016, 2nd Revision May, 27th, 2016, Accepted for publication July 26th, 2016.

Copyright ©2016 Published by ITB Journal Publisher, ISSN: 2337-5779, DOI: 10.5614/j.eng.technol.sci.2016.48.4.1

seawater (used as feed for desalination plants) and they are also contaminated with several chemicals utilized during the desalination process. Spent brine regenerant is a brine effluent that comes from ion-exchange processes and is polluted with resins, multivalent ions of softening plants or organic contaminants [6-8]. Meanwhile, ballast water is seawater containing wide varieties of microorganisms, which may conflict with the different ecological environments wherein it is discharged [9].

Although brine effluents have a negative impact on the environment, they are commonly discharged without any further treatment. Because of more rigorous environmental regulations, industries have started to focus on waste minimization and options to reuse their wastewater, especially brine wastewater. In order to be reused, waste brine should be treated with suitable techniques to obtain the desired water quality. Moreover, brine effluents are also considered as a potential source for valuable uses that may bring cost minimization. In the case of rejected brine from desalination processes, the brine can be treated in a dual-purpose plant that performs simultaneous water recovery and salt production. The sale of the salt product could reduce the net cost of the overall process. Several integrated desalination processes (dominated by the application of advanced membrane-based processes) have been proposed to achieve this promising and interesting dual-purpose scheme of simultaneous desalination and salt production processes [10,11]. This paper is organized to cover several brine effluents and approaches of brine management according to their characteristics.

2 Sources and Characteristics of Brine Effluent

Brine effluents contain a high concentration of salt generated through various processes. Evaporation and concentration of seawater are typical examples of processes that produce brine as effluent. Brine solutions are also utilized in industrial processes for various purposes. However, due to contamination during the process, the brine solutions are generally disposed directly as effluent, without any further treatment. Some types of brines along with their typical characteristics are summarized in Table 1.

Rejected brine from desalination plants contains a high concentration of salt (usually higher than that of its original feed water) and also chemicals imparted during the desalination operations. Another type of brine is the spent brine regenerants that are produced by ion-exchange plants during the regeneration process. Its characteristics depend on the components adsorbed by the resins and also the initial salt concentration.

Types	Characteristics (components) and sources	References
• Rejected brine from desalination plant	• High salt concentration (TDS > 40 g/L) and hardness, containing heavy metals and chemical compounds used in process (anti-scalant, cleaning agent, etc.), higher temperature than ambient (employed in thermal-based processes such as MSF)	[5, 12]
• Spent brine regenerant	• High salinity (about 50 g/L or higher), hardness, and organic compound content (example: decolorization plants)	[13, 14]
 Blow-down water 	• High salinity, TSS, and TOC content (example: SAGD evaporator and boiler with TDS of 50-300 g/L)	[15, 16]
• Rejected bittern brine from salt ponds	• High salinity (up to 400 g/L, mostly contains Na, Mg, K, Br, etc.)	[17]
• Ballast water	 Seawater containing aquatic species including micro- organisms, seaweeds, micro-algae, small invertebrates, eggs, spores, seeds, cysts and larvae of various aquatic plants and animal species 	[18]

 Table 1
 Typical characteristics of Brine Effluent.

Notes: SAGD – *steam assisted gravity drainage; TDS* – *total dissolved solids; TSS* – *total suspended solids; MSF* – *multi-stage flash distillation; TOC* – *total organic carbons*

Meanwhile, in the production of heavy oils and bitumen resources, steamassisted gravity drainage (SAGD) is generally utilized to reduce bitumen viscosity and increase oil production [19,20]. During the oil production process, water is generated while the earth is being drilled. The produced water is recycled and treated for use as boiler-feed water. Due to solute build-up during the recycling process, boiler blow down is required. Usually, the blown down water from SAGD is trucked and disposed into deep wells resulting in high operating costs, which could be the second largest production cost next to the oil production cost [15].

Solar ponds or solar salterns are traditionally employed to produce salt from seawater. During the evaporation process, various salts are precipitated in different stages, whereby the brine remaining in the ponds mainly contains magnesium chloride (MgCl₂) after NaCl precipitation [21]. The remaining brine (known as bittern salt) is usually considered a byproduct. The disposal of the bittern brine is not considered a serious environmental issue since it can be treated to recover valuable components [22]. It can be further processed to recover magnesium, potassium, bromide, boron, and other constituents as valuable products [23].

Although ballast water does not contain a high concentration of salt compared to several counterparts in Table 1, it is also considered a brine effluent. Ballast water is carried by ships to ensure stability, trim and structural integrity during the journey of the ships [24]. Usually ballast water is pumped into the ballast tanks when a ship has delivered cargo to a port and departs with less or no cargo. The ballast water is discharged again when the ship loads cargo. It is taken from one location and can be discharged into other environments that are highly likely to have different ecosystems. Since the microorganisms, algae, seaweeds, etc. in the ballast water are different from those in the original environment, this may pose an ecological threat to the location where the ballast water is discharged. Therefore, the ballast water should be treated first to eliminate any microorganisms it carries.

Brine effluents are also generated by processing of foods, such as canned meat, pickled vegetables, dairy products or fish and by leather industries [25]. In the food industry, brine effluent is generated during canning and pickling. Pickling, chromium tanning or soak liquor generated in the leather industry may contain about 80 g/L of NaCl [25]. The brine effluents generated in these industries are heavily polluted with organic substances. Therefore, the treatment of these brine effluents must be focused on organic compound removal.

3 Brine Discharge Impact

Roberts, *et al.* [26] classified the impact of brine disposal into physiochemical and ecological impacts. The physicochemical impact is attributed to their salinity, temperature and constituents that could alter the physicochemical properties of the receiving water. This alteration may have adverse effects on marine life. For example, elevated salinity of the receiving water body could be harmful for organisms due to the change of the water's osmotic pressure. Consequently, it could change the equilibrium osmotic condition between the water and the organisms, which can damage the cells of the organisms. The brine may also contain toxic components such as heavy metals that may harm aquatic organisms.

Hoepner, *et al.* [27] have reported a case study of the chemical impact of a seawater desalination plant at the northern Red Sea. The effects of chlorine (employed in RO membranes as anti-biofouling agent) and copper in the brine are considered a serious environmental issue, associated with the high toxicity of chlorine and the accumulation of copper in the sediment. Meanwhile, the content of anti-scaling agents in the brine is also of great concern due to their low degradability. Furthermore, a study has pointed out that beach erosion should be taken into consideration for assessing the environmental impact of brine discharge into the sea from coastal desalination plants [1] as brine outfall contributes to beach erosion. Mohamed, *et al.* [28] investigated the impact of brine disposal from inland desalination to the soil and groundwater. They reported that improper disposal of reject brine (particularly its disposal into

unlined ponds or pits) could result in creating pollution of the ground water and soil. The increase of salinity due to intrusion may reduce plant and soil productivity.

In the case of spent brine regenerant from the ion-exchange softening process, the brine contains multivalent ions. The discharge of the spent brine regenerant into a disposal well requires attention to the scaling tendencies in plumbing systems. Anti-scaling agent should be incorporated during the injection of the brine, which increases the cost of discharge. Meanwhile, spent brine containing organic matter can hardly be treated in conventional sewage systems [29]. The high concentration of salts also causes problems for biological activities, so salt-tolerant microorganisms are required to digest the organic substances in the spent brine.

Aquatic bio-invasions that cause impacts to receiving ecosystems during ballast water discharge have been reviewed in the literature [18]. For example, some cholera epidemics (due to the *Vibrio cholera* bacteria) are seen as the result of ballast water discharge. Another example of the adverse effect of improper discharge of ballast water is algae blooming. This may cause massive killing of marine life through oxygen depletion or release of toxic components (depending on the species and the toxicity of the algae).

Due to its environmental impact, regulations have been introduced to set standards for brine discharge. The regulations and salinity limits for desalination brine discharge in some countries have been reviewed by Jenkins *et al.* [30]. According to this report, each country has a different standard, with the lowest incremental salinity limit ≤ 1 ppt. Meanwhile, regulations for ballast water have been provided by the International Maritime Organization (IMO). The regulations outline the ballast water performance standard, which states the limits of specific organisms, such as < 1 cfu/100 mL of toxigenic *Vibrio cholera* and < 250 cfu/100 mL of Escherichia coli, etc. [31]. These regulations are provided to avoid environmental impact of brine discharge.

4 Brine Management

4.1 Brine Discharge Options

Brine discharge options are tabulated in Table 2, classified into the following methods: (1) direct discharge; (2) energy-intensive discharge; (3) evaporation-treated discharge; and (4) land applications. From these options, it can be clearly observed that direct discharge, especially surface water discharge, incurs relatively low capital, operation and maintenance costs. On the other hand, some additional treatments may need to be applied in order to mitigate the

potential impact of surface discharge, such as blending, mixing zone, use of non-toxic chemicals, pH adjustment, and diffusers [32]. If an existing wastewater treatment system is close to the plant, sewer disposal would be an interesting alternative, since its discharge requires low cost and energy. However, the components of brine can reduce the ability of biological processes to treat the organic compounds when a large volume of brine is discharged into the wastewater treatment system [33]. For large amounts of disposed brine (larger than sewer discharge), deep-well injection is suitable, especially for inland desalination systems. However, deep-well injection comes with high capital costs, it is likely to contaminate the groundwater, and it may trigger earthquakes [22].

Table 2	Brine	discharge	options	[33-39]	l
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Classification	Options
Direct discharge	Surface discharge into: lake, reservoir, ocean, river
	Sewer discharge
	Deep-well injection
Energy-intensive	Brine concentrator
discharge	Crystallizer
	Spray dryer
Evaporation-	Evaporation pond
treated discharge	Solar evaporation
	Wind-aided intensification of evaporation (WAIV) technology
Land application	Irrigation of salt tolerant crops and grasses
	Fish farming
	Spirulina cultivation

Due to the disadvantages of direct discharge of brine, the methods of treating brine by applying thermal or related energies are emerging. Evaporation ponds are relatively easy to construct, require little labor to operate, require no mechanical equipment except for pumps, thus bearing low maintenance and operation costs [37]. However, they require a large area of land and thus result in very high capital costs. Moreover, since solar energy is used, the technique relies on appropriate ambient temperatures and is climate-dependent. Leakage due to inappropriate liners of the ponds also potentially has an impact on the environment.

To overcome the problems of solar evaporation ponds, WAIV (wind-aided intensification of evaporation) technology was developed as an alternative. The WAIV method exploits wind energy to evaporate wetted surfaces that are packed at a high density per footprint [38,40]. This method is based on vertically mounted and continuously wetted evaporation surfaces at 20 m^2/m^2 or higher packing densities. By using WAIV technology, the evaporation capacity

is increased to more than 10 times over natural evaporation ponds, thus reducing the footprint of the land area required [38].

To push the limits of minimizing the amount of discharge brine, the zero liquid discharge (ZLD) method has emerged. It employs brine concentrator, crystallizer or spray dryer to recover solid contents from brine [34]. However, since the ZLD system for brine application is complex, consumes a huge amount of energy, and incurs high capital costs, it is not widely applied in industries [34].

Besides the direct and energy-intensive brine discharge methods, land application, or irrigation discharge, has also been developed, although its application is quite limited. It depends solely on land availability, local climate, vegetation tolerance to salinity and the location of the groundwater table [32]. Furthermore, the number of plant types that can grow in high salinity water conditions is very limited, not to mention the salinization of soil that may pose a serious constraint for large-scale application of this method.

4.2 Brine Treatment Methods

4.2.1 Treatment of Brine Effluent from Desalination Process

To reduce the negative environmental impacts of direct brine discharge, brine effluents are repurposed by some advanced treatments (most of which are membrane-based techniques) with several objectives, as summarized in Table 3. The new purposes for the rejected brine from desalination plants are water recovery, salt recovery or salt production, recovery of valuable metals, and other beneficial uses of the brine. In so doing, water recovery is conducted simultaneously with salt production in a dual-purpose plant [41]. As more water is recovered in the recovery process, more concentrated brine is generated, which is suitable for salt manufacture.

For example, Tanaka, *et al.* [42] reported the application of electrodialysis (ED) in salt production by using brine discharge from a SWRO (seawater reverse osmosis) plant. An ED unit was utilized as a pre-concentrator installed before the evaporator. The results of this study showed that energy consumption in the salt manufacturing process using brine discharged from a SWRO plant was 80% from that of the energy consumed in the process using seawater (in other words, it imparts a 20% cost reduction). ED reversal (EDR) has been proposed to control fouling due to precipitation of calcium and magnesium on the ion-exchange membrane [43]. In EDR, the polarity is reversed periodically to pull back the foulant from the membrane. By using this scenario, EDR can improve the degree of salt saturation up to 360% and improve total water recovery in

combination with RO. However, ED is still subject to further improvement to reduce energy consumption in order to meet industrial requirements.

Membrane distillation (MD) is another potential alternative for water recovery and salt production. MD can recover water from brine with high purity and produce a solution containing a high solute concentration simultaneously (Figure 1). However, the major challenge of MD applications is the fouling due to the precipitation of organic or inorganic components that instantaneously reduce membrane permeability. There are cases where fouling occurs in MD during the treatment of brine from an RO plant due to the precipitation of calcium on the membrane. This can be easily washed away by using water [44], but it is also possible that the fouling causes permanent damage to the membrane [45]. Another challenge of the MD process is the wetting phenomenon. This phenomenon can increase mass transfer resistance. Recently, many modifications of membrane surface characteristics have been reported [46,47]. The use of a membrane with high hydrophobicity is expected to suppress the wetting phenomenon in the MD process.

Besides salt, seawater also contains valuable metals that can be recovered for profitable use. However, the development of the processes to extract these metals is still in progress due to difficulties in targeting the selected components. In addition, the process is very complex and requires multiple sequential steps [48,49].

Iodine and its derivative compounds have a high economic value due to their various applications in many different industries. Brine from desalination plants may also contain iodine, which may be recovered as a valuable byproduct [50]. Brine water consists of iodine in the form of an iodide salt. Therefore, oxidation of the iodide ions is required to obtain iodine. The oxidation of iodide to iodine using ozone as oxidation agent in the membrane contactor used as contacting device has shown promising results for iodine recovery from brine [51]. Compared to conventional contacting devices, the membrane contactor has some advantages, such as better contacting performance, larger interfacial area, and ease of direct scale-up [52,53]. With these advantages, this method could potentially be interesting for recovering iodine from brine.

Another membrane technology application with future potential is in the field of power generation from the salinity gradient between seawater or brine disposal and fresh water by using pressure-retarded osmosis (PRO) and reverse electrodialysis (RED) [54]. PRO uses a semi-permeable membrane that allows the transport of water from a low-concentration solution (such as a river, brackish or treated waste water) into a high-concentration draw solution (sea



water) [55]. Energy is generated by using a hydro-turbine in which the kinetic energy of the flowing water is converted to electricity.

Figure 1 Direct contact MD (DCMD) for recovery of waste brine from MSF: (a) schematic of DCMD and (b) flux and product of DCMD in various feed concentrations (feed velocity = 0.5 m/s; permeate velocity = 0.07 m/s; feed temperature = 90° C; permeate temperature = 35° C) [56,57].

In RED, a number of anion and cation exchange membranes are stacked together in an alternating pattern between anode and cathode to allow the selective transport of salt ions [58]. Due to the salinity gradient of the two different solutions fed into the RED cells, chemical potential is converted to electrical potential by transporting ions from the high salinity solution to the low salinity solution. Integrated SWRO-PRO and SWRO-RED are promising processes to alleviate water and energy demands. Post, *et al.* [59] compared the power density and energy recovery performances of PRO and RED by mixing different types of saline water, i.e. seawater and brine, with river water. They showed that higher potential maximum power density could be achieved with RED (2-4 W/m²) than with PRO (1.2-1.5 W/m²) when these membranes are applied in seawater and river water. When applied to brine water, the PRO membrane seems to be more attractive with its higher power density and energy recovery (up to 15 W/m²) [60]. By using these methods, not only electricity can be generated but also the salt concentration of the brine can be reduced.

To achieve the purpose of ZLD and the dual purpose of simultaneous desalination and salt production, several integrated desalination processes have been proposed. These processes yield zero or near zero liquid discharge, increased water recovery, and profitable salt production that can be used to offset the overall fresh water production cost. They include a combined membrane-thermal desalination process and an integrated membrane processes. As shown in Figure 2, which analyzes the costs of both production of fresh water and salt (in \$/m³) by using integrated processes, it can be seen that Scheme 2 consisting of MF/NF/RO/MCr (microfiltration, nanofiltration, reverse osmosis, and membrane crystallization) is the most feasible scheme due to the profit generated by the salt sale, which is higher than the cost of fresh-water production.



Figure 2 Cost of fresh-water production and salts sale per water produced by different integrated processes. Scheme 1: MF/NF/RO; Scheme 2: MF/NF/RO/MCr; Scheme 3: ED/EDR; Scheme 4: UF/NF/MSF/crystallization; Scheme 5: UF/NF/RO/MSF/crystallization; Scheme 6: ED/MSF/crystallization. Data collected from [11,43,61,62].

4.2.2 Treatment of Spent Brine Regenerant

The most promising alternative for handling spent brine regenerant is brine reuse. The technologies that can be used for this purpose are chemical precipitation, nanofiltration membranes (NF), biological treatment, and membrane bioreactor processing (Table 3). The chemical precipitation process (using sodium hydroxide) consists of several steps, including precipitation, neutralization using acid, and salt make-up [63]. As reported in the literature [63,64], chemical precipitation has the following advantages: reduction of regeneration and waste brine costs by almost 90% in comparison to waste hauling (thus rendering waste hauling unnecessary) and delivering significantly reduced cost of water for regeneration. Meanwhile, the chemical cost is slightly increased compared to that of sewer disposal due to alkaline solution consumption for precipitation. Overall, chemical precipitation gives a satisfactory cost for brine disposal treatment in ion-exchange softening plants. It should be noted that supplementary clarifier is needed for the precipitation process. A large volume of clarifier may be needed if this process is going to be used for treatment of large volumes of brine.

Nanofiltration (NF) is a membrane-based process with high rejection towards bivalent and multivalent ions while providing low to moderate rejection for monovalent ions, which is useful for regeneration of spent brine from softening plants. Due to its capability of removing organic substances, NF may also be used for brine regeneration in decolorization plants or other brine contaminated with organic components [65]. However, due to the high concentration of the brine, additional acidification or an anti-scaling injection is required. Furthermore, NF requires high pressure to drive the high flux and rejection.

Purpose	Technologies	References			
Rejected brine from desalination plant					
Water recovery	• CDI, ED, EDR, FO, MD, VESEP	[44, 66-70]			
• Water and salt recovery (salt production)	• ED, MD, MCr, SAL-PROC process	[42, 71-73]			
• Beneficial reuse (HCl and NaOH production)	• Bipolar membrane ED (BMED)	[74]			
• Recovery of valuable metals (P, Ce, Cs, In, Ge, etc.)	• Extraction and adsorption	[48,49]			
• Energy generation and brine dilution	• RED, PRO	[75, 76]			
Spent brine regenerant					
 Partial reuse and discharge 	 Partial recycling 	[63]			
Water reuse	• RO MD	[13, 77]			

 Table 3
 Brine effluent treatment: purposes and technologies.

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Purpose	Technologies	References
Brine reuse	 Chemical precipitation, NF, biological treatment, MBR 	[14,64,78-80]
Ballast water		
• Physical treatment	 Crum rubber filtration, micro-pore ceramic filtration, hydrocyclone, UV, heat treatment, ultrasound, GloEn-Patrol TM system 	[81-87]
• Chemical treatment	 Ozone, ClO₂, NaOCl, Seakleen[®], ParaClean[®] ocean 	[88-92]
Electro-chemical treatment	 Electrolysis 	[24]
 Advanced oxidation process 	• UV/Ag-TiO ₂ +O ₃	[93]
Combined treatment	 Micro-pore ceramic + filtration + UV; hydrocyclone + chemical disinfectant 	[82,94]

 Table 3 Continued. Brine effluent treatment: purposes and technologies.

Note: CDI - capacitive de-ionization; ED - electrodialysis; EDR - electrodialysis reversal; RED - reversed electrodialysis; FO - forward osmosis; MD - membrane distillation; MCr - membrane crystallization; NF - nanofiltration; PRO - pressure retarded osmosis; RO - reverse osmosis; UV - ultraviolet; VESEP - vibratory shear enhanced process.

Membrane bioreactor (MBR) processing combines conventional activated sludge and membrane separation processes. Applications of MBR for spent brine regeneration have been reported in [78]. Despite of the excellent performance in the removal of organic content, fouling remains a main drawback of the process. Numerous strategies have been studied to minimize membrane fouling [95-99]. With the developed control of fouling in the MBR process, MBR could be a promising alternative for spent brine regeneration, particularly for treatment of brine that is heavily polluted with organic compounds.

4.2.3 Ballast Water Treatment

Ballast water treatment technologies can be categorized as physical treatment, chemical treatment, electrochemical treatment, advanced oxidation, and combined treatment (Table 3). Despite the excellent elimination of harmful organisms, these methods still suffer from several drawbacks. For example, UV irradiation requires high energy consumption, the equipment needs to be cleaned periodically, and the lamps are fragile and break easily [100-102]. In addition, UV irradiation is not effective for removal of large organisms and highly depends on the clarity of the water [103]. On the other hand, the electrolysis of ballast water can generate byproducts, especially hydrogen gas (H₂) that has a potential risk of explosion, and the performance is affected by various conditions such as salinity [104]. Oxidizing methods such as chlorination and ozonation can promote the generation of disinfection by products (DBPs) when the disinfectant reacts with chloride and bromide, as

presented in [105]. Sonication is effective to remove zooplankton up to 90%, but it is inefficient for the removal of phytoplankton with size < 100 μ m [86]. Chemical treatments may also produce various byproducts, while excess chemicals could potentially promote water pollution. Therefore, new alternative methods for treating ballast water are under development, including combined methods to obtain more efficient ballast water treatment.

5 Conclusion

Several approaches have been proposed to provide strategies for brine handling that are oriented at minimizing waste effluent by recovering both brine and water, or to remove pollutant components so it may comply with environmental regulations while being discharged. The dual-purpose desalination and salt production plant is a promising strategy for both rejected brine handling and reducing the total cost of pure water production in a desalination plant. Spent brine regeneration and reuse can be beneficial approaches dealing with spent brine from the ion-exchange regeneration process. Meanwhile, appropriate technologies are required to eliminate harmful organisms from ballast water such as filtration, advanced oxidation, or combined integrative treatments. Furthermore, advanced membrane-based approaches have been summarized and analyzed from an economic point of view as a sustainable alternative for treating various brine effluents.

References

- Al-Barwani, H.H. & Purnama, A., *Re-assessing the Impact of Desalination Plants Brine Discharges on Eroding Beaches*, Desalination. 204, pp. 94-101, 2007.
- [2] Al-Handhaly, J.K., Mohamed, A.M.O. & Maraqa, M., Impact of Chemical Composition of Reject Brine from Inland Desalination Plants On Soil and Groundwater, UAE, Desalination, 156, p. 89, 2003.
- [3] Einav, R., Harussi, K. & Perry, D., *The Footprint of the Desalination Processes on the Environment*, Desalination, **152**. pp. 141-154, 2003.
- [4] Fernández-Torquemada, Y., Sánchez-Lizaso, J.L. & González-Correa, J.M., *Preliminary Results of the Monitoring of the Brine Discharge Produced by the SWRO Desalination Plant of Alicante (SE Spain)*, Desalination, **182**, pp. 395-402, 2005.
- [5] Hashim, A. & Hajjaj, M., Impact of Desalination Plants Fluid Effluents on the Integrity of Seawater, with the Arabian Gulf in Perspective, Desalination, 182, pp. 373-393, 2005.
- [6] Brigano, F.A., Souce, W.J. & Rak, S.F., *Reclaiming of Spent Brine*, US Patent 5,254,257, 1993.

- [7] McAdam, E.J. & Judd, S.J., Biological Treatment of Ion-Exchange Brine Regenerant for Re-Use: A Review, Separation and Purification Technology, 62, pp. 264-272, 2008.
- [8] Kabsch-Korbutowicz, M., Wisniewski, J., Łakomska, S. & Urbanowska, A., Application of UF, NF and ED in Natural Organic Matter Removal from Ion-Exchange Spent Regenerant Brine, Desalination, 280, pp. 428-431, 2011.
- [9] King, D.M. & Tamburri, M.N., Verifying Compliance with Ballast Water Discharge Regulations, Ocean Development & International Law, 41, pp. 152-165, 2010.
- [10] Ravizky, A. & Nadav, N., Salt Production by the Evaporation of SWRO Brine in Eilat: A Success Story, Desalination, 205, pp. 374-379, 2007.
- [11] Turek, M., Seawater Desalination and Salt Production in A Hybrid Membrane-Thermal Process, Desalination, 153, pp. 173-177, 2003.
- [12] Ahmed, M., Shayya, W.H., Hoey, D. & Al-Handaly, J., Brine Disposal from Reverse Osmosis Desalination Plants in Oman and The United Arab Emirates, Desalination, 133, pp. 135-147, 2001.
- [13] Gryta, M., Karakulski, K., Tomaszewska, M. & Morawski, A., Treatment of Effluents from the Regeneration of Ion Exchangers Using the MD Process, Desalination, 180, pp. 173-180, 2005.
- [14] Wadley, S., Brouckaert, C.J., Baddock, L.A.D. & Buckley, C.A., Modelling of Nanofiltration Applied to the Recovery of Salt from Waste Brine at a Sugar Decolourisation Plant, Journal of Membrane Science, 102, pp. 163-175, 1995.
- [15] Saltworks, Case Study: SAGD Blowdown, http://saltworkstech.com/wpcontent/uploads/2015/01/Saltworks_Case-Study_SAGD-Blowdown_EN. pdf, (19 May 2015).
- [16] Maiti, A., Sadrezadeh, M., Guha Thakurta, S., Pernitsky, D.J. & Bhattacharjee, S., Characterization of Boiler Blowdown Water from Steam-Assisted Gravity Drainage and Silica–Organic Coprecipitation During Acidification and Ultrafiltration, Energy & Fuels, 26, pp. 5604-5612, 2012.
- [17] Baati, H., Jarboui, R., Gharsallah, N., Sghir, A. & Ammar, E., Molecular Community Analysis of Magnesium-Rich Bittern Brine Recovered from a Tunisian Solar Saltern, Canadian Journal of Microbiology, 57, pp. 975-81, 2011.
- [18] Gonçalves, A.A. & Gagnon, G.A., Recent Technologies for Ballast Water Treatment, Ozone: Science & Engineering, 34, pp. 174-195, 2012.
- [19] Bagci, S., The Effect of Fractures on The Steam-Assisted Gravity Drainage Process, Energy & Fuels, 18, pp. 1656-1664, 2004.
- [20] Giacchetta, G., Leporini, M. & Marchetti, B., Economic and Environmental Analysis of a Steam Assisted Gravity Drainage (SAGD)

Facility for Oil Recovery from Canadian Oil Sands, Applied Energy, **142**, pp. 1-9, 2015.

- [21] Folchitto, S., Seawater as Salt and Water Source for Solar Ponds, Solar Energy, 46, pp. 343-351, 1991.
- [22] Ahmad, N. & Baddour, R.E., A Review of Sources, Effects, Disposal Methods, and Regulations of Brine Into Marine Environments, Ocean & Coastal Management, 87, pp. 1-7, 2014.
- [23] Nayaka, N. & Pandab, C.R., Determination of Major and Trace Elements in Bittern for Possible Value Addition, International Journal of Energy and Environmental Engineering, 1, pp. 8-12, 2014.
- [24] Lacasa, E., Tsolaki, E., Sbokou, Z., Rodrigo, M.A., Mantzavinos, D. & Diamadopoulos, E., *Electrochemical Disinfection of Simulated Ballast Water on Conductive Diamond Electrodes*, Chemical Engineering Journal, 223, pp. 516-523, 2013.
- [25] Lefebvre, O. & Moletta, R., Treatment of Organic Pollution in Industrial Saline Wastewater: A Literature Review, Water Research, 40, pp. 3671-3682, 2006.
- [26] Roberts, D.A., Johnston, E.L. & Knott, N.A., Impacts of Desalination Plant Discharges on the Marine Environment: A Critical Review of Published Studies, Water Research, 44, pp. 5117-5128, 2010.
- [27] Hoepner, T. & Lattemann, S., Chemical Impacts from Seawater Desalination Plants - a Case Study of the Northern Red Sea, Desalination, 152, pp. 133-140, 2003.
- [28] Mohamed, A.M.O., Maraqa, M. & Al Handhaly, J., Impact of Land Disposal of Reject Brine from Desalination Plants on Soil and Groundwater, Desalination, 182, pp. 411-433, 2005.
- [29] Barranco, C.R., Balbuena, M.B., García, P.G.A. & Fernández, A.G., Management of Spent Brines or Osmotic Solutions, Journal of Food Engineering, 49, pp. 237-246, 2001.
- [30] Jenkins, S., Paduan, J., Roberts, P., Schlenk, D. & Weis, J., Management of Brine Discharges to Coastal Waters. Recommendations of A Science Advisory Panel, Technical Report 694, The Southern California Coastal Water Research Project, Costa Mesa, CA, March, 2012.
- [31] Gollasch, S., David, M., Voigt, M., Dragsund, E., Hewitt, C. & Fukuyo, Y., Critical Review of the IMO International Convention on the Management of Ships' Ballast Water and Sediments, Harmful Algae, 6, pp. 585-600, 2007.
- [32] Younos, T., Environmental Issues of Desalination, Journal of Contemporary Water Research & Education, 132, pp. 11-18, 2005.
- [33] Xu, P., Cath, T.Y., Robertson, A.P., Reinhard, M., Leckie, J.O. & Drewes, J.E., *Critical Review of Desalination Concentrate Management*, *Treatment and Beneficial Use*, Environmental Engineering Science, 30, pp. 502-514, 2013.

- [34] Brandhuber, P., Cerone, J., Kwan, P., Moore, E. & Vieira, A., A Look at Conventional and Emerging Brine Disposal and Waste Minimization Technologies, Waterscapes, 19, pp. 7-10, 2008.
- [35] Afrasiabi, N. & Shahbazali, E., RO *Brine Treatment and Disposal Methods*, Desalination and Water Treatment, **35**, pp. 39-53, 2011.
- [36] Voutchkov, N., Overview of Seawater Concentrate Disposal Alternatives, Desalination, 273, pp. 205-219, 2011.
- [37] Ahmed, M., Shayya, W.H., Hoey, D., Mahendran, A., Morris, R. & Al-Handaly, J., Use of Evaporation Ponds for Brine Disposal in Desalination Plants, Desalination, 130, pp. 155-168, 2000.
- [38] Gilron, J., Folkman, Y., Savliev, R., Waisman, M. & Kedem, O., WAIV-Wind Aided Intensified Evaporation for Reduction of Desalination Brine Volume, Desalination, 158, pp. 205-214, 2003.
- [39] Sánchez, A.S., Nogueira, I.B.R. & Kalid, R.A., Uses of the Reject Brine from Inland Desalination for Fish Farming, Spirulina Cultivation, and Irrigation of Forage Shrub and Crops, Desalination, 364, pp. 96-107, 2015.
- [40] Katzir, L., Volkmann, Y., Daltrophe, N., Korngold, E., Mesalem, R., Oren, Y. & Gilron, J., WAIV - Wind Aided Intensified Evaporation for Brine Volume Reduction and Generating Mineral Byproducts, Desalination and Water Treatment, 13, pp. 63-73, 2010.
- [41] Wenten, I.G. & Khoiruddin, Reverse Osmosis Applications: Prospect and Challenges, Desalination, 391, pp. 112-125, 2016.
- [42] Tanaka, Y., Ehara, R., Itoi, S. & Goto, T., Ion-Exchange Membrane Electrodialytic Salt Production Using Brine Discharged from a Reverse Osmosis Seawater Desalination Plant, Journal of Membrane Science, 222, pp. 71-86, 2003.
- [43] Turek, M., Dual-Purpose Desalination-Salt Production Electrodialysis, Desalination, 153, pp. 377-381, 2003.
- [44] Mericq, J.-P., Laborie, S. & Cabassud, C., Vacuum Membrane Distillation of Seawater Reverse Osmosis Brines, Water Research, 44, pp. 5260-5273, 2010.
- [45] Gryta, M., Fouling in Direct Contact Membrane Distillation Process, Journal of Membrane Science, **325**, pp. 383-394, 2008.
- [46] Himma, N.F., Anisah, S., Prasetya, N. & Wenten, I.G., Advances in Preparation, Modification, and Application of Polypropylene Membrane, Journal of Polymer Engineering, 36, pp. 329-362, 2015.
- [47] Himma, N.F., Wardani, A.K. & Wenten, I.G., Preparation of Superhydrophobic Polypropylene Membrane Using Dip-Coating Method: The Effects of Solution and Process Parameters, Polymer-Plastics Technology and Engineering, DOI: 10.1080/03602559.2016.1185666, 2016.

- [48] Le Dirach, J., Nisan, S. & Poletiko, C., Extraction of Strategic Materials from the Concentrated Brine Rejected by Integrated Nuclear Desalination Systems, Desalination, 182, pp. 449-460, 2005.
- [49] Petersková, M., Valderrama, C., Gibert, O. & Cortina, J.L., Extraction of Valuable Metal Ions (Cs, Rb, Li, U) from Reverse Osmosis Concentrate Using Selective Sorbents, Desalination, 286, pp. 316-323, 2012.
- [50] Nabieyan, B., Kargari, A., Kaghazchi, T., Mahmoudian, A. & Soleimani, M., Bench-Scale Pertraction of Iodine Using a Bulk Liquid Membrane System, Desalination, 214, pp. 167-176, 2007.
- [51] Wenten, I.G., Julian, H. & Panjaitan, N.T., Ozonation Through Ceramic Membrane Contactor for Iodide Oxidation During Iodine Recovery from Brine Water, Desalination, 306, pp. 29-34, 2012.
- [52] Purwasasmita, M., Nabu, E.B.P., Khoiruddin & Wenten, I.G., Non Dispersive Chemical Deacidification of Crude Palm Oil in Hollow Fiber Membrane Contactor, Journal of Engineering and Technological Sciences, 47, pp. 426-446, 2015.
- [53] Drioli, E., Curcio, E. & Di Profio, G., State of the Art and Recent Progresses in Membrane Contactors, Chemical Engineering Research and Design, 83, pp. 223-233, 2005.
- [54] Wenten, I.G., Khoiruddin, Aryanti, P.T.P. & Hakim, A.N., Scale-Up Strategies for Membrane-Based Desalination Processes: A Review, Journal of Membrane Science and Research, 2, pp. 42-58, 2016.
- [55] Lee, K.L., Baker, R.W. & Lonsdale, H.K., Membranes for Power Generation by Pressure-Retarded Osmosis, Journal of Membrane Science, 8, pp. 141-171, 1981.
- [56] Viona, V. & Wenten, I.G., Treatment of Multi Stage Flash Distillation Unit's Waste Brine Using Membrane Distillation, The 3rd Regional Symposium on Membrane Science and Technology, Bandung, Indonesia, 2005.
- [57] Wenten, I.G., Reuse of Multi-Stage Flash Waste Brine Using Direct Contact Membrane Distillation, Pertamina, Cilacap, 2005.
- [58] Długołęcki, P., Gambier, A., Nijmeijer, K. & Wessling, M., Practical Potential of Reverse Electrodialysis as Process for Sustainable Energy Generation, Environmental Science & Technology, 43, pp. 6888-6894, 2009.
- [59] Post, J.W., Hamelers, H.V.M. & Buisman, C.J.N., Energy Recovery from Controlled Mixing Salt and Fresh Water with a Reverse Electrodialysis System, Environmental Science & Technology, 42, pp. 5785-5790, 2008.
- [60] Ramon, G.Z., Feinberg, B.J. & Hoek, E.M.V., Membrane-Based Production of Salinity-Gradient Power, Energy & Environmental Science, 4, pp. 4423-4434, 2011.
- [61] Drioli, E., Curcio, E., Di Profio, G., Macedonio, F. & Criscuoli, A., Integrating Membrane Contactors Technology and Pressure-Driven

Membrane Operations for Seawater Desalination: Energy, Exergy and Costs Analysis, Chemical Engineering Research and Design, 84, pp. 209-220, 2006.

- [62] Turek, M., Cost Effective Electrodialytic Seawater Desalination, Desalination, 153, pp. 371-376, 2003.
- [63] Michaud, C.F.C., 'Zero D' A Method of Reducing Industrial Softener Discharge, Water Conditioning & Purification, 52, pp. 26-30, 2010.
- [64] Michaud, C.F.C., Zero Discharge Softener Regeneration, Water Conditioning & Purification, **39**, pp. 40-45, 1994.
- [65] Cartier, S., Theoleyre, M.A. & Decloux, M., Treatment of Sugar Decolorizing Resin Regeneration Waste Using Nanofiltration, Desalination, 113, pp. 7-17, 1997.
- [66] Ng, H.Y., Lee, L.Y., Ong, S.L., Tao, G., Viawanath, B., Kekre, K., Lay, W. & Seah, H., *Treatment of RO Brine-Towards Sustainable Water Reclamation Practice*, Water science and Technology, **58**, pp. 931-936, 2008
- [67] Korngold, E., Aronov, L. & Daltrophe, N., *Electrodialysis of Brine Solutions Discharged from an RO Plant*, Desalination, 242, pp. 215-227, 2009.
- [68] Turek, M., Was, J. & Dydo, P., Brackish Water Desalination in RO-Single Pass EDR System, Desalination and Water Treatment, 7, Pp. 263-266, 2009.
- [69] Martinetti, C.R., Childress, A.E. & Cath, T.Y., High Recovery of Concentrated RO Brines Using Forward Osmosis and Membrane Distillation, Journal of Membrane Science, 331, pp. 31-39, 2009.
- [70] Subramani, A., DeCarolis, J., Pearce, W. & Jacangelo, J.G., Vibratory Shear Enhanced Process (VSEP) for Treating Brackish Water Reverse Osmosis Concentrate with High Silica Content, Desalination, 291, pp. 15-22, 2012.
- [71] Ji, X., Curcio, E., Al Obaidani, S., Di Profio, G., Fontananova, E. & Drioli, E., *Membrane Distillation-Crystallization of Seawater Reverse Osmosis Brines*, Separation and Purification Technology, **71**, Pp. 76-82, 2010.
- [72] Drioli, E., Curcio, E., Criscuoli, A. & Profio, G.D., Integrated System for Recovery of CaCO₃, NaCl and MgSO₄·7H₂O from Nanofiltration Retentate, Journal of Membrane Science, 239, pp. 27-38, 2004.
- [73] Ahmed, M., Arakel, A., Hoey, D., Thumarukudy, M.R., Goosen, M.F.A., Al-Haddabi, M. & Al-Belushi, A., *Feasibility of Salt Production from Inland RO Desalination Plant Reject Brine: A Case Study*, Desalination, 158, pp. 109-117, 2003.
- [74] Badruzzaman, M., Oppenheimer, J., Adham, S. & Kumar, M., Innovative Beneficial Reuse of Reverse Osmosis Concentrate Using Bipolar

Membrane Electrodialysis and Electrochlorination Processes, Journal of Membrane Science, **326**, pp. 392-399, 2009.

- [75] Tufa, R.A., Curcio, E., van Baak, W., Veerman, J., Grasman, S., Fontananova, E. & Di Profio, G., *Potential of Brackish Water and Brine* for Energy Generation by Salinity Gradient Power-Reverse Electrodialysis (SGP-RE), RSC Advances, 4, pp. 42617-42623, 2014.
- [76] Kim, J., Park, M., Snyder, S.A. & Kim, J.H., Reverse Osmosis (RO) and Pressure Retarded Osmosis (PRO) Hybrid Processes: Model-Based Scenario Study, Desalination, 322, pp. 121-130, 2013.
- [77] Ghasemipanah, K., Treatment of Ion-Exchange Resins Regeneration Wastewater Using Reverse Osmosis Method for Reuse, Desalination and Water Treatment, 51, pp. 5179-5183, 2013.
- [78] McAdam, E.J., Pawlett, M. & Judd, S.J., Fate and Impact of Organics in an Immersed Membrane Bioreactor Applied to Brine Denitrification and Ion Exchange Regeneration, Water Research, 44, pp. 69-76, 2010.
- [79] Lien, L.A., Spent Brine Reclamation, US Patent No. 6,004,464, 1999.
- [80] Hiremath, T., Roberts, D.J., Lin, X., Clifford, D.A., Gillogly, T.E.T. & Lehman, S.G., *Biological Treatment of Perchlorate in Spent ISEP Ion-Exchange Brine*, Environmental Science & Technology, 23, pp. 1009-1016, 2006.
- [81] Tang, Z., Butkus, M.A. & Xie, Y.F., Crumb Rubber Filtration: A Potential Technology for Ballast Water Treatment, Marine Environmental Research, 61, pp. 410-423, 2006.
- [82] Liu, S., Zhang, M., Li, X., Tang, X., Zhang, L., Zhu, Y. & Yuan, C., *Technical Feasibility Study of an Onshore Ballast Water Treatment System*, Frontiers of Environmental Science & Engineering, 5, pp. 610-614, 2011.
- [83] Waite, T., Kazumi, J., Lane, P., Farmer, L., Smith, S., Smith, S., Hitchcock, G. & Capo, T., *Removal of Natural Populations of Marine Plankton by a Large-Scale Ballast Water Treatment System*, Marine Ecology Progress Series, 258, pp. 51-63, 2003.
- [84] Kong, X., Zhu, Y., Zhang, M., Sun, X. & Zhang, W., Simulated Experiment on Minimizing the Presence Chlorella and Bacteria in Ballast Water by Combination of Micro-Hole Filtration and UV Radiation, Journal of Advanced Oxidation Technologies, 10, pp. 186-188, 2007.
- [85] Meshabi, E., Norman, R.A., Vourdachas, A. & Qutkez-Badia, G., Design of High-Temperature Thermal Ballast Water Treatment System, Proceedings of the Institution of Mechanical Engineers, Part M: Journal of Engineering for the Maritime Environment, 22, pp. 31-42, 2007.
- [86] Holm, E.R., Stamper, D.M., Brizzolara, R.A., Barnes, L., Deamer, N. & Burkholder, J.M., Sonication of Bacteria, Phytoplankton and

Zooplankton: Application to Treatment of Ballast Water, Marine Pollution Bulletin, **56**, pp. 1201-1208, 2008.

- [87] Jung, Y.J., Yoon, Y., Pyo, T.S., Lee, S.-T., Shin, K. & Kang, J.-W., Evaluation of Disinfection Efficacy and Chemical Formation Using MPUV Ballast Water Treatment System (GloEn-Patrol[™]), Environmental Technology, 33, pp. 1953-1961, 2012.
- [88] Herwig, R.P., Cordell, J.R., Perrins, J.C., Dinnel, P.A., Gensemer, R.W., Stubblefield, W.A., Ruiz, G.M., Kopp, J.A., House, M.L. & Cooper, W.J. Ozone Treatment of Ballast Water on the Oil Tanker S/T Tonsina: Chemistry, Biology and Toxicity, Marine Ecology Progress Series, 324, pp. 37-55, 2006.
- [89] Maranda, L., Cox, A.M., Campbell, R.G. & Smith, D.C., Chlorine Dioxide as a Treatment for Ballast Water to Control Invasive Species: Shipboard Testing, Marine Pollution Bulletin, 75, pp. 76-89, 2013.
- [90] Gray, D.K., Duggan, I.C. & Mac Isaac, H.J., Can Sodium Hypochlorite Reduce the Risk of Species Introductions from Diapausing Invertebrate Eggs in Non-Ballasted Ships? Marine Pollution Bulletin, 52, pp. 689-695, 2006.
- [91] Wright, D.A., Dawson, R., Caceres, V., Orano-Dawson, C.E., Kananen, G.E., Cutler, S.J. & Cutler, H.G., Shipboard Testing of the Efficacy of Seakleen® as a Ballast Water Treatment to Eliminate Non-Indigenous Species Aboard a Working Tanker in Pacific Waters, Environmental Technology, 30, pp. 893-910, 2009.
- [92] La Carbona, S., Viitasalo-Frösen, S., Masson, D., Sassi, J., Pineau, S., Lehtiniemi, M. & Corroler, D., *Efficacy and Environmental Acceptability* of Two Ballast Water Treatment Chemicals and an Alkylamine Based-Biocide, Science of The Total Environment, 409, pp. 247-255, 2010.
- [93] Wu, D., You, H., Zhang, R., Chen, C. & Lee, D.-J., Ballast Waters Treatment Using UV/Ag-TiO₂+O₃ Advanced Oxidation Process With Escherichia Coli and Vibrio Alginolyticus as Indicator Microorganisms, Chemical Engineering Journal, 174, pp. 714-718, 2011.
- [94] Veldhuis, M.J.W., Fuhr, F., Boon, J.P. & Ten Hallers-Tjabbers, C.C., Treatment of Ballast Water; How to Test a System With a Modular Concept? Environmental Technology, 27, Pp. 909-921, 2006.
- [95] Wenten, I.G., Performance of Newly Configured Sumberged Membrane Bioreactor for Aerobic Industrial Wastewater Treatment, Reaktor, 12, pp. 137-145, 2009.
- [96] Wenten, I.G., Koenhen, D.M., Roesink, H.D.W., Rasmussen, A. and Jonsson, G., *The Backshock Process: A Novel Backflush Technique in Microfiltration*, Proceedings of Engineering of Membrane Processes, II Environmental Applications, Ciocco, Italy, 1994.

- [97] Wenten, I.G., *Recent Development in Membrane Science and Its Industrial Applications*, Songklanakarin Journal of Science and Technology, **24**, Pp. 1010-1024, 2002.
- [98] Aryanti, P.T.P., Yustiana, R., Purnama, R.E.D. & Wenten, I.G., *Performance and Characterization of PEG400 Modified PVC Ultrafiltration Membrane*, Membrane Water Treatment, **6**, pp. 379-392, 2015.
- [99] Aryanti, P.T.P., Subagjo, S., Ariono, D. & Wenten, I.G., Fouling and Rejection Characteristic of Humic Substances in Polysulfone Ultrafiltration Membrane, Journal of Membrane Science and Research, 1, pp. 41-45, 2015.
- [100] Boldor, D., Balasubrama, S., Purohit, S. & Rusch, K.A., Design and Implementation of a Continuous Microwave Heating System for Ballast Water Treatment, Environmental Science & Technology, 42, pp. 4121-4127, 2008.
- [101] Mamlook, R., Badran, O., Abu-Khader, M., Holdo, A. & Dales, J., Fuzzy Sets Analysis for Ballast Water Treatment Systems: Best Available Control Technology, Clean Technologies and Environmental Policy, 10, pp. 397-407, 2008.
- [102] Zhang, Y., Bai, M., Chen, C., Meng, X., Tian, Y., Zhang, N. & Yu, Z., OH Treatment for Killing of Harmful Organisms In Ship's Ballast Water with Medium Salinity Based on Strong Ionization Discharge, Plasma Chemistry and Plasma Processing, 33, pp. 751-763, 2013.
- [103] Perakis, A.N. & Yang, Z., Options for Nonindigenous Species Control and Their Economic Impact on The Great Lakes and St. Lawrence Seaway: A Survey, Marine Technology, 40, Pp. 34-41, 2003.
- [104] Bai, M., Zhang, Z., Zhang, N., Tian, Y., Chen, C. & Meng, X., Treatment of 250 t/h Ballast Water in Oceanic Ships Using OH Radicals Based on Strong Electric-Field Discharge, Plasma Chemistry and Plasma Processing, 32, pp. 693-702, 2012.
- [105] Hayes, K.R. & Sliwa, C., Identifying Potential Marine Pests-A Deductive Approach Applied to Australia, Marine Pollution Bulletin, 46, pp. 91-98, 2003.